TEST REPORT

REPORT NUMBER: G100248857MID-006R
REPORT DATE: April 22, 2011
REVISED DATE: April 27, 2011

EVALUATION CENTER
Intertek Testing Services NA Inc.
8431 Murphy Drive
Middleton, WI 53562

RENDERED TO

Dectra Corporation
3425 33rd Avenue, NE
Saint Anthony, MN 55418

PRODUCT EVALUATED:

Model WHS1500VV Solid Fuel Hydronic Furnace

Report of Testing Model WHS1500V Solid Fuel Hydronic Heater for compliance with the applicable requirements of the following criteria: Appendix X1 Modified test method for wood-fired hydronic appliances that utilize thermal storage of ASTM E2618-09 Measurement of particulate emissions and heating efficiency of outdoor solid fuel-fired hydronic heating appliances.

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APPENDICES

REVISION SUMMARY

DATE	SUMMARY
April 27, 2011	Revised model designation to indicate that model WHS1500V was tested. Also added model WHS1500H as a similar model.

I. INTRODUCTION

I.A. GENERAL

From March 28, 2011 to April 1, 2011 Intertek Testing Services NA Inc. (Intertek) conducted tests on the WHS1500V Solid Fuel Hydronic Heater to determine emission and efficiency results for Dectra Corporation.

Tests were conducted by Ken Slater at the Dectra Corporation facility located at 1162 Red Fox Road, Arden Hills, Minnesota. Tests were evaluated to the Appendix X1 Modified test method for wood-fired hydronic appliances that utilize thermal storage for ASTM E2618-09 Standard Test Method for Measurement of Particulate Emissions and Heating Efficiency of Outdoor Solid Fuel-Fired Hydronic Heating Appliances.

I.B. TEST UNIT DESCRIPTION

The model WHS1500V is a solid fueled unit with a 14.15 cubic foot firebox and is constructed of carbon sheet steel and weighs 3140 lbs. dry. The heat exchanger extends through the water vessel, which holds 11574 lbs. of water.

I.C. RESULTS

The unit as tested produced an average emissions rate of:
0.130 lbs/million Btu of output for the heating season
0.131 lbs/million Btu of output for year round

I.D. PRETEST INFORMATION

The unit was inspected upon arrival at the Dectra Corporation facility and found to be in good condition. The unit was set up per the manufacturer's instructions. The unit was placed on the test stand and instrumented with thermocouples in the specified locations. The chimney system and laboratory dilution tunnel was cleaned using standard wire brush chimney cleaning equipment.

On March 29, 2011, the unit was ready for testing.

II. SUMMARY OF TEST RESULTS

II.A EPA Results

CAT	Load % Capacity	Tgt Load (Btu/hr)	Act Load (Btu/hr)	Test Duration (Hours)	WoodWt (Lb)	Q_{in} (Btu)	Q_{out} (Btu)	η_N (%)	E_T (g)	E (g/MJ)	E Output (lb/mmbtu)	E Input (lb/mmbtu)	E (g/hr)
I	<15% of max	37,500	37,500	2.79	119.8	1,024,504	685,641	66.9%	41.3	0.06	0.13	0.089	2.26
II	16 – 24% of max	50,000	50,000	2.79	119.8	1,024,504	695,203	67.9%	41.3	0.06	0.13	0.089	2.97
III	25 -50% of max	93,750	93,750	2.79	119.8	1,024,504	709,048	69.2%	41.3	0.06	0.13	0.089	5.46
IV	Max capacity	250,000	250,000	2.79	119.8	1,024,504	719,279	70.2%	41.3	0.05	0.13	0.089	14.35

Average BTU/hr for 8 hr. burn time	**88,519**

II.B

Heating Season Weighting

	Weighting			Input	Output	
Cat	**Factor**	$\eta \times F_i$	$E_{g/MJ,I} \times F_i$	$E_{lb/mmbtu} \times F_i$	$E_{lb/mmbtu} \times F_i$	$E_{g/hr} \times F_i$
I	0.175	0.117	0.010	0.023	0.016	0.395
II	0.275	0.187	0.015	0.036	0.024	0.817
III	0.450	0.311	0.025	0.058	0.040	2.456
IV	0.100	0.070	0.005	0.013	0.009	1.435
Totals	1.000	**69%**	**0.06**	**0.130**	**0.09**	**5.10**

II.C

Year Round Use Weighting

	Weighting			Input	Output	
Cat	**Factor**	$\eta \times F_i$	$E_{g/MJ,I} \times F_i$	$E_{lb/mmbtu} \times F_i$	$E_{lb/mmbtu} \times F_i$	$E_{g/hr} \times F_i$
I	0.437	0.29	0.025	0.06	0.04	0.99
II	0.238	0.16	0.013	0.03	0.02	0.71
III	0.275	0.19	0.015	0.04	0.02	1.50
IV	0.050	0.04	0.003	0.01	0.00	0.72
Totals	1.000	**68%**	**0.06**	**0.131**	**0.09**	**3.91**

Efficiency

Category	**HHV**	**LHV**
I	66.9%	76.5%
II	67.9%	77.6%
III	69.2%	79.1%
IV	70.2%	80.3%

II.D Summary of other Data

	Run 2	Run 3	Run 4	Standby	Units
Steel Mass	3140	3140	3140	3140	lbs
Water Mass	11574	11574	11574	11574	lbs
Fuel Load Weight	144.13	144.76	143.75		lbs
Fuel MC (dry basis)	22.30250006	23.4836534	21.39409855		%
Kindling Mass	2.14	2.24	2.2		lbs
Kindling MC (dry basis)	10	10	10		%
Starting system temp.	126.649094	128.31515	126.214094	172.00	F
Ending System Temp.	188.1	187.38839	188.802938	165.4	F
Average Room Temp.	65.94	66.41741	65.62081	66.37	
Burn Time	164	170	168		Minutes
Burn Time	2.73	2.83	2.80		Hours
Standby Test Duration				19	Hours
HHV	8550	8550	8550		BTU/lb
Dry Fuel Weight	54	54	55		Kg
Burn Rate	19.89	19.10	19.51		Kg/hr
Input	1,024,227	1,019,728	1,029,557		BTU
Heat Stored	730,528	702,263	744,056		BTU
Average	730,528	702,263	744,056		
Standby Loss Rate				25.7	BTU/hr-F
Total Emissions	39.81	44.29	39.75		Grams
Total Emissions	0.088	0.098	0.088		lbs
Category I Output Rate	37500	37500	37500	2183	BTU/hr
Category II Output Rate	50000	50000	50000	2183	BTU/hr
Category III Output Rate	93750	93750	93750	2183	BTU/hr
Category IV Output Rate	250000	250000	250000	2183	BTU/hr
Output Time Cat I	18.4	17.7	18.7		Hours
Output Time Cat II	14.0	13.5	14.3		Hours
Output Time Cat III	7.6	7.3	7.8		Hours
Output Time Cat IV	2.9	2.8	3.0		Hours
				Average	
Category I Efficiency	67.4%	65.1%	68.3%	66.9%	
Category II Efficiency	68.3%	66.0%	69.2%	67.9%	
Category III Efficiency	69.7%	67.3%	70.6%	69.2%	
Category IV Efficiency	70.7%	68.3%	71.6%	70.2%	

Category I Emissions	0.127	0.147	0.125	0.13	lbm/mmBTU output
Category II Emissions	0.125	0.145	0.123	0.13	lbm/mmBTU output
Category III Enissions	0.123	0.142	0.120	0.13	lbm/mmBTU output
Category IV Emissions	0.121	0.140	0.119	0.13	lbm/mmBTU output

III. PROCESS DESCRIPTION

III.A. DISCUSSION

RUN #2 (March 30, 2011). The starting temperature in the heat storage vessel was 127^{o}F. Burn time was 2.73 hours and ended with a heat storage vessel temperature of 188^{o}F.

RUN #3 (March 31, 2011). The starting temperature in the heat storage vessel was 128^{o}F. Burn time was 2.83 hours and ended with a heat storage vessel temperature of 187^{o}F.

RUN #4 (April 1, 2011). The starting temperature in the heat storage vessel was 126^{o}F. Burn time was 2.80 hours and ended with a heat storage vessel temperature of 189^{o}F.

III.B. UNIT DIMENSIONS

Overall dimensions are 71.75-in wide, 96-in deep, 71.5-in high.

III.C. AIR SUPPLY SYSTEM

Combustion air enters the unit in the front of the unit aided by a combustion air blower. Combustion air is controlled electronically. This air is directed to the Firebox. Combustion products flow through a heat exchanger system. Combustion products exit through a 6-in flue collar located at the top back of the outer enclosure.

III.D. OPERATION DURING TEST

The boiler is operated until the entire fuel load is consumed and there is no further combustion in the firebox. The end of the test is determined when the water storage temperature is no longer increasing.

III.E TEST FUEL PROPERTIES

The fuel used was Quercus Ruba L. (Oak, Red). The fuel was split cordwood with dimensions around 4-in thick x 4-in long x 16-in in length. The fuel was dried to average moisture content between 19% and 25% on a dry basis.

III.F. START-UP OPERATION

The cordwood fuel started with newspaper and a measured kindling load. As the test load was being lit, the sampling system was started simultaneously. The unit was allowed to operate until all combustion in the firebox had ceased.

IV. SAMPLING SYSTEMS

The ASTM E2515-2007 sampling procedure was used.

IV.A. SAMPLING LOCATIONS

Particulate samples are collected from the dilution tunnel at a point 16 feet from the tunnel entrance. The tunnel has two elbows ahead of the sampling section. (See Figure 3.) The sampling section is a continuous 14-foot section of 10-inch diameter pipe straight over its entire length. Tunnel velocity pressure is determined by a standard Pitot tube located 96 inches from the beginning of the sampling section. The dry bulb thermocouple is located six inches downstream from the Pitot tube. Tunnel samplers are located 36 inches downstream of the Pitot tube and 36 inches upstream from the end of this section. (See Figure 1.)

IV.A.(1) DILUTION TUNNEL

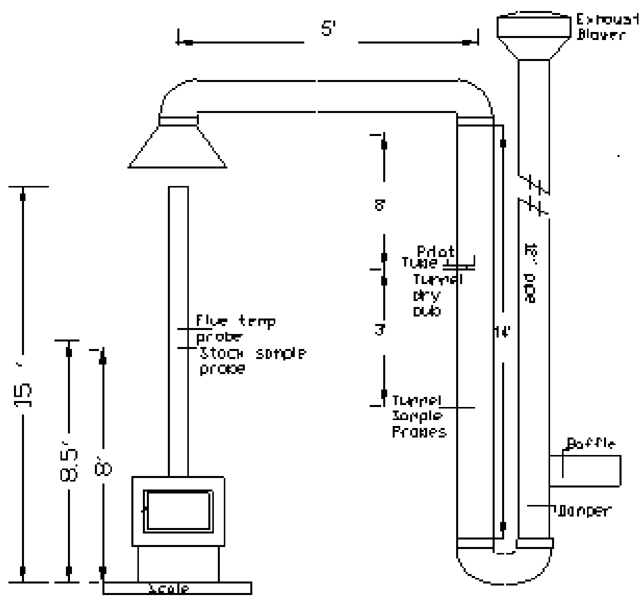

FIGURE 1

IV.B.OPERATIONAL DRAWINGS

IV.B.(2). DILUTION TUNNEL SAMPLE SYSTEMS

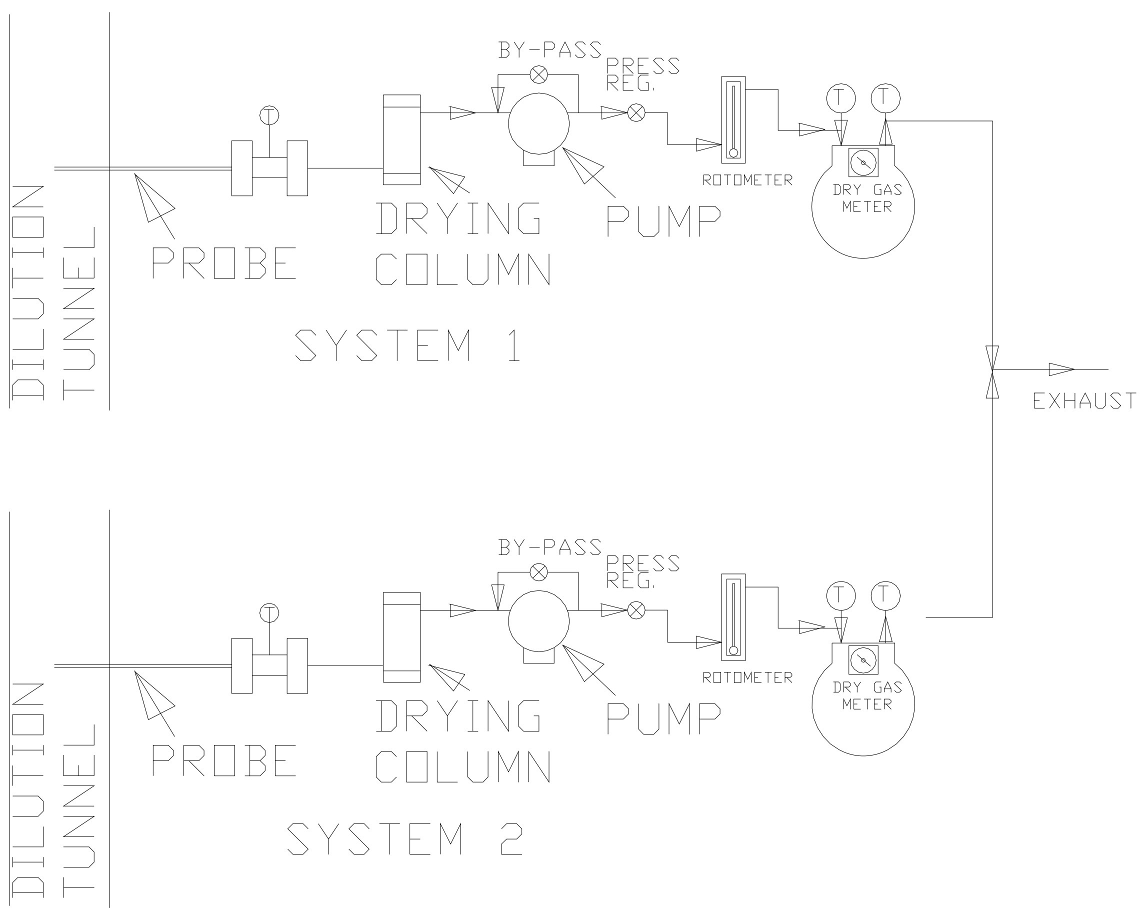

Figure 2

V. SAMPLING METHODS

V.A. PARTICULATE SAMPLING

Particulates were sampled in strict accordance with ASTM E2515-09. This method uses two identical sampling systems with Gelman A/E 61631 binder free, 47-mm diameter filters. The dryers used in the sample systems are filled with “Drierite” before each test run.

VI. QUALITY ASSURANCE

VI.A. INSTRUMENT CALIBRATION

VI.A. (1). DRY GAS METERS

At the conclusion of each test program the dry gas meters are checked against our standard dry gas meter. Three runs are made on each dry gas meter used during the test program. The average calibration factors obtained are then compared with the six-month calibration factor and, if within 5%, the six-month factor is used to calculate standard volumes. Results of this calibration are contained in Appendix D.

An integral part of the post test calibration procedure is a leak check of the pressure side by plugging the system exhaust and pressurizing the system to 10” W.C. The system is judged to be leak free if it retains the pressure for at least 10 minutes.

The standard dry gas meter is calibrated every 6 months using a Spirometer designed by the EPA Emissions Measurement Branch. The process involves sampling the train operation for 1 cubic foot of volume. With readings made to .001 ft^3, the resolution is .1%, giving an accuracy higher than the ±2% required by the standard.

VI.A.(2). STACK SAMPLE ROTOMETER

The stack sample rotometer is checked by running three tests at each flow rate used during the test program. The flow rate is checked by running the rotometer in series with one of the dry gas meters for 10 minutes with the rotometer at a constant setting. The dry gas meter volume measured is then corrected to standard temperature and pressure conditions. The flow rate determined is then used to calculate actual sampled volumes.

VI.B. TEST METHOD PROCEDURES

VI.B.(1). LEAK CHECK PROCEDURES

Before and after each test, each sample train is tested for leaks. Leakage rates are measured and must not exceed 0.02 CFM or 4% of the sampling rate. Leak checks are performed checking the entire sampling train, not just the dry gas meters. Pre-test and post-test leak checks are conducted with a vacuum of 10 inches of mercury. Vacuum is monitored during each test and the highest vacuum reached is then used for the post test vacuum value. If leakage limits are not met, the test run is rejected. During, these tests the vacuum was typically less than 2 inches of mercury. Thus, leakage rates reported are expected to be much higher than actual leakage during the tests.

VI.B.(2). TUNNEL VELOCITY/FLOW MEASUREMENT

The tunnel velocity is calculated from a center point Pitot tube signal multiplied by an adjustment factor. This factor is determined by a traverse of the tunnel as prescribed in EPA Method 1. Final tunnel velocities and flow rates are calculated from EPA Method 2, Equation 6.9 and 6.10. (Tunnel cross sectional area is the average from both lines of traverse.)

Pitot tubes are cleaned before each test and leak checks are conducted after each test.

VI.B.(3). PM SAMPLING PROPORTIONALITY (5G-3)

Proportionality was calculated in accordance with EPA Method 5G-3. The data and results are included in Appendix C.

VII RESULTS AND OBSERVATIONS

The Model WHS1500V has been found to be in compliance with the applicable performance and construction requirements of the following criteria:
"**Appendix X1 Modified test method for wood-fired hydronic appliances that utilize thermal storage of ASTM E2618-09 Measurement of particulate emissions and heating efficiency of outdoor solid fuel-fired hydronic heating appliances**"

The model WHS1500V was the model tested, which is configured with a vertical flue located at the top back of the unit. Model WHS1500H is an identical model with the only difference being that the flue exits horizontally out the back of the unit. The model WHS1500H does contain slightly more water in the vessel due to the flue area is not notched out for the vertical flue exit.

INTERTEK TESTING SERVICES NA

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